

Process Intensification and Green Chemistry – Notation and Symbolology

Chapter 3 (process intensification)

Roman symbol	Definition	Units	Comments
a	surface area per unit volume	m^2/m^3	
A	area	m^2	
A	amplitude	m	
A/V	surface area of heat transfer to reaction volume	$1/\text{m}$	
ATU	area of a transfer unit	m^2	ATU takes the form of A_G , A_L , A_{OG} , or A_{OL} depending on which film is controlling
B^o	nuclei formed per unit volume per unit time	$1/\text{m}^3/\text{s}$	
Bo	Bodenstein number	-	
c	molar concentration of solute in solution	mol/m^3	
c^*	molar equilibrium concentration (solubility)	mol/m^3	
C_D	discharge coefficient of baffle	-	
C_W	flow rate coefficient	-	
d	diameter of disk	m	
d	inner tube diameter	m	
d_e	effective diameter of multi-orifice COBRs	m	if number of orifices $n_o = 1$, $d_e = d$
d_o	orifice diameter	m	
D or D_m	diffusion coefficient	m^2/s	
E_{ML}	Murphree efficiency based on liquid phase	-	
E_{MV}	Murphree efficiency based on vapor phase	-	
f	frequency	Hz	
F	F -factor	$\text{Pa}^{0.5}$	
F_V or F	feed flow rate	m^3/s	
G	molar flow rate of gaseous/vapor phase	mol/s	
G	crystal growth rate	m/s	
G	Gap ratio (RS-SDR)	-	
h	convective heat transfer coefficient	$\text{W}/\text{m}^2/\text{K}$	
$HETP$	height equivalent of a theoretical plate	m	
k	mass transfer coefficient	m/s	

k	thermal conductivity	W/m/K	
k_G	crystal growth rate constant	various units	function of temperature, agitation speed, impurities and system
k_L	mass transfer coefficient	m/s	
$k_L a$	volumetric mass transfer coefficient	1/s	
k_N	nucleation rate constant	various units	function of temperature
l	characteristic crystal length	m	
l_e	mixing length for eddy enhancement model	m	
L	molar flow rate of liquid phase	mol/s	
L	Baffle spacing (COBR)	m	
L/d	length to internal tube diameter ratio	-	
M_T	slurry density	various units	
n_o	number of orifices	-	
N	agitation speed	rpm	
N_b	number of baffles per unit length		
N_{CSTR}	number of CSTRs in series for the tank-in-series model		parameter used to characterize the non-ideality of real reactors
Nu	Nusselt number		
NTP	number of equilibrium plates		
NTS	number of equilibrium stages		
NTU	number of transfer units		NTU takes the form of N_G , N_L , N_{OG} , or N_{OL} depending on which film is controlling
p	pressure	Pa	
P	power	W	
Pr	Prandtl number		
Pe_{ax}	axial Peclet number		
Q	volumetric flow rate	m ³ /s	
\dot{Q}	heat flow	W	
r	radial distance	m	
R	disk radius (TF-SDR)	m	
r_d	disk radius (RS-SDR)	m	
r_i	inner radius	m	
r_o	outer radius	m	
Re	Reynolds number		
Re_n	net flow Reynolds number		equivalent to Re
Re_o	oscillatory Reynolds number		
s	gap between rotor and stator (RS-SDR)	m	

s	supersaturation	mol/m ³	
S	saturation ratio		
Str or Sr or St	Strouhal number		
t	time	s	
t_{mx}	mixing time	s	
T	oscillation period	s	
T	temperature	°C or K	
u	velocity	m/s	
u_G	velocity of gas phase	m/s	
U	overall heat transfer coefficient	W/m ² /K	
v	velocity	m/s	
v_r	radial velocity	m/s	
v_θ	tangential velocity	rad/s	
V	volume	m ³	
V_r	volume of reactor	m ³	
V_{PFR}	plug flow volume	m ³	
V_{PFR}^*	volume fraction of plug flow to total reactor volume		
W	electrical power	W	
x	mole fraction of solute in bulk liquid phase		
x_i	mole fraction of solute in liquid phase at vapor/liquid interface		
x_j	mole fraction of solute in liquid phase at position j		j can refer to F feed, B bottoms, D distillate, or positions 1 or 2 of RPB
x_0	center-to-peak amplitude	m	
X	molar conversion		
y	mole fraction of solute in bulk vapor phase		
y_i	mole fraction of solute in vapor phase at vapor/liquid interface		
y_j	mole fraction of solute in vapor phase at position j		j can refer to F feed, B bottoms, D distillate, or positions 1 or 2 of RPB
z	position	m	
Greek symbols	Definition	Units	Comments
α	open cross-sectional area	m ²	
$\dot{\gamma}(r, z)$	shear rate	1/s	
$\delta(r)$	film thickness	m	
$\bar{\delta}$	mean film thickness	m	
ε	specific power dissipation or energy dissipation rate	W/m ³ or W/kg	
η	internal effectiveness factor		
λ	thermal conductivity	W/m/K	
μ	dynamic viscosity	Pa s	

ν	kinematic viscosity	m ² /s
$\nu_{i,j}$	stoichiometric coefficient of species i in reaction j	
ρ_G	density of the gas phase	kg/m ³
$\overline{\rho_m}$	mean density	kg/m ³
σ^2	variance	
$\sigma^2(\dot{\gamma})$	variance in the shear rate	1/s ²
$\sigma^2(\varepsilon)$	variance in the specific power dissipation	W ² /m ⁶
τ	mean residence time	s
τ_c	contact time (penetration theory)	s
τ_{mx}	(micro)mixing time	s
τ_{rx}	reaction time	s
ϕ	Thiele modulus	
Ψ	velocity ratio	
ω	angular velocity	rad/s
Ω	overall effectiveness factor	
Abbreviation	Definition	
CAPEX	capital expenditure	
CFD	computational fluid dynamics	
COBC	continuous oscillatory baffled crystallizer	
COBR	continuous oscillatory baffled reactor	
CSD	crystal size distribution	
CSTR	continuous stirred tank reactor	
HETP	height equivalent to a theoretical plate	
HEX	heat exchanger reactor	
HGAP	high-gravity anti-solvent precipitation	
HTF	heat transfer fluid	
MSMPR	mixed suspension mixed product removal	
MSZW	metastable zone width	
OPEX	operating expenditure	
PI	process intensification	
RPB	rotating packed bed	
RSR or RS-SDR	rotor-stator spinning disk reactor	
RTD	residence time distribution	
RZB	rotating zigzag bed	
SDR	spinning disk reactor	
SS	stainless steel	

TF-SDR	thin-film spinning disk reactor
TSCC-RPB	two-stage counter-current rotating packed bed